

UNITS		Design Equations (gas phase)		Design Equations (liquid phase)	
Variables	Units	CSTR	PFR	CSTR	PFR
temperature	kelvin	$V=(F_{Ao}X)/-r_a$	$dF_a/dV=r_a$	$V=(F_{j0}-F_j)/-r_j$	$r_j=dF_j/dV$
activation energy	joules	$F_{Ao}=C_{Ao}v_o$	$F_a=F_{Ao}(1-X)$	$V=(v_oC_{j0}-vC_j)/-r_j$	$V=F_{j0} \int_0^X \frac{dF_j}{r_j}$
volume	1 dm <sup>3</sup> = 1 liter	$V=(C_{Ao}v_oX)/-r_a$	$dF_a=d(-F_{Ao}(1-X))=-F_{Ao}dX \Rightarrow F_a=C_{Ao}(dX/dt)V=-r_aV$	$V^{isom}=v_o(C_{Ao}-C_a)/kCa$	$r_a=dF_a/dV$ , $F_a=VC_a$
concentration	moles/liter			$V=(F_{Ao}X)/-r_a$	$r_a=(d(v_o^*C_a))/dV$
Design Equations (liquid phase)				$V=(C_{Ao}v_oX)/(k^*Ca)$	$V^{first order}=C_{Ao}v_o \int_0^X \frac{1}{kC_{Ao}^*(1-X)} dX$
PBR	BR	$C_{Ao}=N_{Ao}/v_o$ $=P_{Ao}/R T_o=(y_{Ao}P_o)/R^*T_o$	$dV=F_{Ao} \int_0^X \frac{dX}{-r_a}$ $>0 \Rightarrow V \int_0^X \frac{dV}{V}$		
$dF_j/dw=r_j'$	$dN_a/dt=r_aV$	$V=(y_{Ao}P_o v_o X)/(R T_o^* r_a)$	$0 \rightarrow X \int_0^X \frac{F_{Ao} dX}{-r_a}$ $>X \int_0^X \frac{dX}{-r_a}$		
$w=F_{j0} \int_0^X \frac{dF_j}{r_j'}$	$N_a(t)=N_{Ao}(1-X(t))$			$V=(v_o^*X)/(k(1-X))$	
$w=(F_{j0}-F_j)/r_j'$	$N_{Ao}(dX/dt)=-r_aV$			Activation Energy	
	$t=N_{Ao} \int_0^X \frac{dX}{-r_aV}$			$k=Ae^{-E_a/RT}$	
Random Shit I need to Know				$\ln k = \ln A - (E_a/RT)$	
$PV=nRT \Rightarrow n/V=C_t$ $\rho=P/RT$	$-r_a=k(C_a^2C_b - C_c/K_c)$		<b>PBR</b>	$E_a = (R \ln(k_2/k_1))/(1/T_1 - 1/T_2)$	
$C_{j0} = y_{j0} C_{t0}$	$k_c=C_c/(C_a^2C_b)$		$F_{Ao}(dX/dw)=-r_a'$		
$C_a=(C_{Ao}(1-X))/(1+\epsilon X)$	$-r_a=0$ @ equilibrium		$W=F_{Ao} \int_0^X \frac{dX}{-r_a'}$		
$C_b=(C_{Ao}(\theta_b - (b/a)X))/(1+\epsilon X)$					
$C_c=(C_{Ao}(\theta_c + (c/a)X))/(1+\epsilon X)$					
$C_i=C_{i0}/(1+\epsilon X)$					
Conversion					
		$X=X_a$ =moles of A reacted/moles of A fed in= $(N_{Ao}-N_a)/N_{Ao}$			
		$N_a=N_{Ao}(1-X)$			
		$F_a=F_{Ao}(1-X)$			
		$C_a=C_{Ao}(1-X)$			

